



Interplay of Pd ensemble sites induced by GaO_x modification in boosting CO₂ hydrogenation to formic acid

Kohsuke Mori^{a,b,*}, Hiroto Hata^a, Hiromi Yamashita^{a,b,*}

^a Division of Materials and Manufacturing Science, Graduate School of Engineering, Osaka University, 2-1 Yamada-oka, Osaka 565-0871, Japan

^b Innovative Catalysis Science Division, Institute for Open and Transdisciplinary Research Initiatives (ICS-OTRI), Osaka University, Suita, Osaka 565-0871, Japan

ARTICLE INFO

Keywords:

Surface engineering
Nanoparticle
Gallium oxide
Formic acid
Carbon dioxide

ABSTRACT

The interfacial modification of Pd nanoparticles supported on *g*-C₃N₄ (CN) was performed using highly dispersed amorphous MO_x phase, where M represents Ga, Al, or B. The resulting Pd@MO_x/CN exhibited enhanced activity in the hydrogenation of CO₂ to yield formic acid. In particular, Pd@GaO_x/CN displayed a maximum turnover number of 4540 based on the quantity of surface-exposed Pd atoms; this turnover number is more than six times higher than that of the unmodified catalyst. DFT calculations show that the presence of GaO_x clusters on the Pd (111) surface produces the unique Pd ensemble sites, where electron-deficient Pd^{δ+} and electron-rich Pd^{δ-} are adjacent. On the basis of kinetic and theoretical investigations, we propose a reasonable dual activation mechanism: the electron-deficient Pd^{δ+} species facilitates the adsorption of HCO₃⁻ ions, whereas the electron-rich Pd^{δ-} species accelerates not only H₂ dissociation but also the attack of dissociated H atoms on C atoms in HCO₃⁻ ions.

1. Introduction

The hydrogenation of CO₂ to formic acid (FA; HCOOH) is of significant interest not only because CO₂ is an inexpensive, nontoxic, abundant C1 feedstock but also because FA is considered to be a renewable hydrogen storage material due to its relatively high hydrogen content (53 g·L⁻¹), low toxicity, and nonflammable characteristics [1–5]. The gas-phase hydrogenation of CO₂ to produce FA has a positive free energy change ($\Delta G = +33 \text{ kJ}\cdot\text{mol}^{-1}$) [6], but this reaction proceeds more readily in aqueous solution ($\Delta G = -4 \text{ kJ}\cdot\text{mol}^{-1}$) [7]. This reaction is typically performed with the addition of a weak base (B), which shifts the thermodynamic equilibrium to the product side: CO₂ (aq) + H₂ (aq) + B → HCO₂⁻ (aq) + BH⁺, $\Delta G = -35.4 \text{ kJ}\cdot\text{mol}^{-1}$ [8]. Significant efforts have been devoted to the research of homogeneous transition metal complexes in basic media, and some of these catalytic systems have proven extremely efficient [9–11]. Unfortunately, advancements in reliable heterogeneous catalysts for FA synthesis via CO₂ hydrogenation have lagged behind [5,12–14].

We previously investigated a series of supported PdAg nanoparticle (NP) catalysts, such as random PdAg, Pd@Ag, and Ag@Pd, on TiO₂ prepared using surface engineering approaches with atomic precision [15]. A strong correlation has been demonstrated between increased

catalytic activity and increased electron negativity of active Pd atoms due to a synergy between effects originating from Pd and Ag. Kinetic and density functional theory (DFT) calculations demonstrated that this synergistic effect boosts the attack on the C atom in adsorbed HCO₃⁻ at a positively charged Ag site by a dissociated H atom at a negatively charged Pd site. These results provide advanced insight into a possible design strategy for catalytically active sites for CO₂ hydrogenation to FA [16].

In nano-engineering, an ongoing challenge in the field of catalyst design, the angstrom-scale and nanoscale architecture of NPs plays a dominant role in determining their efficiency and selectivity [17–19]. Control of particle size is essentially utilized to tune the concentration of low-coordination sites and surface vacancies, allowing effective utilization of expensive catalyst metals [20–22]. Special nanostructures such as rods, cubes, and polycrystals are known to exert a strong influence on catalytic activity and selectivity due to differences in the preferential exposure of particular crystallographic planes [23–25]. The utilization of the strong metal–support interaction between metal NPs and catalyst supports frequently leads to unique synergistic effects at their interfaces, which further influence particle size and the overall size distribution of metal NPs [26–28]. Surface modification with organic ligands not only inhibits the aggregation of metal NPs but also controls

* Correspondence to: 1-2 Yamadaoka, Graduate School of Engineering, Osaka University, Osaka, 565-0871, Japan.

E-mail addresses: mori@mat.eng.osaka-u.ac.jp (K. Mori), yamashita@mat.eng.osaka-u.ac.jp (H. Yamashita).

<https://doi.org/10.1016/j.apcatb.2022.122022>

Received 17 August 2022; Received in revised form 23 September 2022; Accepted 26 September 2022

Available online 27 September 2022

0926-3373/© 2022 Elsevier B.V. All rights reserved.

the adsorption kinetics of reactants or intermediates through specific geometric effects or metal–ligand electronic effects [29–32]. In alloys with second and third metals, the coordination of one metal to another can provide novel active sites and often alters electronic properties, endowing catalytic activity and selectivity superior to those of mono-metallic counterparts [33–36].

In this study, we utilized highly dispersed MO_x phase (where M represents a group 13 element, namely, Ga, Al, or B) as inorganic ligands to alter the electronic state of surface Pd NPs, with the aim of improving catalytic performance during CO_2 hydrogenation to produce FA. Unlike organic ligands, which exhibit Lewis basicity, the oxide (O_2^-) moieties of MO_x ligands connect with metal centers to form extended structures. In these structures, specific group 13 metal ions influence its coordinating ability and ultimately determine catalytic performance. Modification with GaO_x produced a maximum turnover number based on the quantity of surface exposed Pd atoms, which is six times higher than that of the unmodified Pd catalyst. Such enhancement is attributed to the interplay of unique Pd ensemble sites with the aid of associated MO_x ligands. In this interplay, the electron-deficient $\text{Pd}^{\delta+}$ species facilitates the adsorption of HCO_3^- ions, whereas the electron-rich $\text{Pd}^{\delta-}$ species accelerates not only H_2 dissociation but also the attack of dissociated H atoms on C atoms in HCO_3^- ions, as evidenced by kinetic and DFT calculations.

2. Experimental section

2.1. Materials

Na_2PdCl_4 was obtained from Tokyo Kasei Kogyo Co., Ltd. Melamine, $\text{Ga}(\text{NO}_3)_3 \cdot n\text{H}_2\text{O}$, and $\text{Al}(\text{NO}_3)_3 \cdot 0.9 \text{H}_2\text{O}$ were purchased from Nacalai Tesque. H_3BO_3 and NaHCO_3 were purchased from Wako Pure Chemical Industries, Ltd. All commercially available compounds were used as received. Distilled water was employed as the reaction solvent.

2.2. Synthesis of GaO_x -modified Pd/g- C_3N_4 (Pd@ GaO_x/CN)

g- C_3N_4 was prepared according to a previously reported procedure [37]. Melamine of 30 g was heated in a muffle furnace in air at 550 °C for 4 h to give a yellow solid. The solid was crushed into powder in a mortar. The obtained g- C_3N_4 (0.5 g) was dispersed in 100 mL of an aqueous solution containing Na_2PdCl_4 (0.047 mmol) and $\text{Ga}(\text{NO}_3)_3 \cdot n\text{H}_2\text{O}$ (0.047 mmol), followed by stirring at room temperature for 1 h. The suspension was evaporated under vacuum. Subsequently, the sample was reduced with NaBH_4 (0.28 mmol) to yield Pd@ GaO_x/CN (Pd, 1.0 wt%; Pd/Ga molar ratio = 1/1). Pd@ AlO_x/CN and Pd@ BO_x/CN were prepared with the same method using $\text{Al}(\text{NO}_3)_3 \cdot 0.9 \text{H}_2\text{O}$ and H_3BO_3 , respectively. Metal loadings were determined using inductively coupled plasma (ICP) analysis. The catalysts can be synthesized with high reproducibility.

2.3. General procedure for the catalytic hydrogenation of CO_2

CO_2 hydrogenation to FA was conducted with a batch reactor system using a stainless steel autoclave (60 mL). In each trial, the catalyst (10 mg) and a 1.0-M aqueous NaHCO_3 solution (15 mL) were transferred into the reactor, and the pressure was set to 2.0 MPa by adding H_2 and CO_2 in a 1:1 molar ratio. The system was subsequently heated to 100 °C and stirred for 6 h. FA yields were determined with high-performance liquid chromatography at 40 °C using a Shimadzu instrument equipped with a Bio-Rad Aminex HPX-87 H ion exclusion column (300 × 7.8 mm) with 5-mM H_2SO_4 (0.5 mL/min) as the mobile phase. TON values were determined by dividing the quantity of FA produced after 6 h by the moles of total Pd or surface-exposed Pd, as appropriate.

2.4. Characterization

Powder XRD patterns were recorded using a Rigaku Ultima IV diffractometer with Cu K_α radiation ($\lambda = 1.54056 \text{ \AA}$). Nitrogen

adsorption–desorption isotherms were acquired at $-196 \text{ }^\circ\text{C}$ using a BELSORP-max system (MicrotracBEL Corp.). Samples were degassed at 150 °C for 3 h under vacuum to vaporize physisorbed water prior to each trial. Specific surface areas were calculated using the BET method using nitrogen adsorption data. Metal concentrations in the samples were determined using ICP-AES analysis with a Nippon Jarrell-Ash ICAP-575 Mark II instrument. TEM images were obtained with a Hitachi H-800 instrument operating at 200 kV. STEM images and elemental maps were obtained using a JEOL-ARM 200 F apparatus equipped with a KveX energy-dispersive X-ray detector (JED-2300 T) operating at 200 kV. CO pulse adsorption was performed by using a BEL-METAL-1 instrument (BEL Japan, Inc.) to measure the Pd dispersion. The sample was pre-treated under He flow at 323 K for 15 min and subsequently under H_2 flow at 323 K for 60 min. The CO adsorption was measured at 323 K using 1%CO/He at a flow rate of 20 mL·min^{−1}. Pd and Ga K-edge XAFS spectra were recorded using a fluorescence yield collection technique with a Si(111) monochromator at the 01B1 beamline station at the SPring-8 facility, JASRI, Harima, Japan (proposal nos. 2020A0523 and 2020A1062). Data reduction was performed using the REX2000 software program (Rigaku). To obtain radial structure functions, Fourier transformation of the k^3 -weighted normalized EXAFS data was carried out over the range $3.0 \text{ \AA} < k/\text{\AA}^{-1} < 12 \text{ \AA}$. Temperature programmed reduction with H_2 (H_2 -TPR) was conducted using a BEL-CAT (BEL Japan, Inc.) instrument by heating 30 mg samples at $5 \text{ }^\circ\text{C min}^{-1}$ from -100 – $300 \text{ }^\circ\text{C}$ under a 5.0% H_2/Ar flow. The H_2 - D_2 exchange reaction was monitored using a BELCATII system (MicrotracBEL Corp.). After the pretreatment under He flow at 323 K for 30 min, the H_2 - D_2 exchange reaction was performed at 323 K using 25% H_2/He and 25% D_2/He at a flow rate of 25 mL·min^{−1}. Products (H_2 , HD and D_2) were analyzed with an online mass spectrometer. The rate constant was determined from the produced HD amount.

2.5. DFT calculations

All DFT calculations were performed with the DMol³ program in the Materials Studio 17.2 software package [38,39]. The generalized gradient approximation exchange–correlation functional proposed by Perdew, Burke, and Ernzerhof was combined with the double numerical basis set plus polarization functions. A supercell slab consisting of a surface 5×5 unit cells with three atomic (111) surface layers was adopted. For the calculation, periodic boundary conditions were applied to the slabs. The reactant atoms and their adjacent atoms were relaxed during geometry optimizations, and the other layers were fixed at the corresponding bulk positions. Transition states (TSs) were determined using the nudged elastic band method, and the activation energy was defined by the energy difference between the TS and reactant.

3. Results and discussion

3.1. Characterization of Pd@ GaO_x/CN

The deposition of metal catalysts was performed using a conventional method. Briefly, g- C_3N_4 [Brunauer–Emmett–Teller (BET) surface area $S_{\text{BET}} = 7.5 \text{ m}^2 \cdot \text{g}^{-1}$] was impregnated with an aqueous solution of Na_2PdCl_4 and $\text{Ga}(\text{NO}_3)_3 \cdot n\text{H}_2\text{O}$. The Pd/Ga ratio in the resulting material was controlled by varying the concentration of Ga while maintaining a constant Pd loading of 1.0 wt%. The samples obtained in this manner were subsequently reduced with NaBH_4 without calcination, yielding Pd@ GaO_x supported on g- C_3N_4 (i.e., Pd@ GaO_x/CN) with various Pd/Ga atomic ratios. The same impregnation method was used to synthesize Pd@ AlO_x/CN and Pd@ BO_x/CN along with $\text{Al}(\text{NO}_3)_3 \cdot 0.9 \text{H}_2\text{O}$ and H_3BO_3 precursors as the second metals, followed by reduction with NaBH_4 .

The X-ray diffraction (XRD) pattern of Pd@ GaO_x/CN exhibited peaks due to Pd(111) and Pd(200) at 40.2° and 47.0° , respectively, with no characteristic peaks assignable to PdGa intermetallic alloy (Fig. S1). X-ray photoelectron spectroscopy (XPS) analysis showed that the peak of

the Ga 3d spectrum of Pd@GaO_x/CN could be deconvoluted with the main peak centered at 20.3 eV and the minor peak centered at 19.1 eV, which reflects Ga³⁺ (95.7%) and Ga²⁺ (6.3%), respectively (Fig. S2). No peak due to metallic Ga was observed. Significant differences were not observed in the N₂ adsorption–desorption isotherms of the material before and after metal deposition ($S_{\text{BET}} = 9.7 \text{ m}^2 \cdot \text{g}^{-1}$ for Pd@GaO_x/CN) (Fig. S3). Pd@AlO_x/CN and Pd@BO_x/CN also showed similar S_{BET} .

The shapes of the Pd K-edge X-ray absorption near-edge structure (XANES) spectra of Pd/CN and Pd@MO_x/CN (M = Ga, Al, or B) differed from those of the Pd foil but resembled those of PdO with two distinct peaks attributed to the allowed 1s–5p transition (Fig. 1a). More detailed inspection verified the differences in the shape at approximately 24,385 eV in the comparison of Pd/CN with Pd@MO_x/CN (M = Ga, Al, or B), indicating that the symmetry of the Pd metal face centered cubic structure was slightly disordered by integration with MO_x (M = Ga, Al, or B) [18]. In the Fourier-transform extended X-ray absorption fine structure (FT-EXAFS) spectra at the Pd K-edge of each sample, the peak due to the Pd–O and/or Pd–N bond and that due to contiguous metallic Pd–Pd bonds were observed at approximately 1.6 and 2.5 Å, respectively (Fig. 1b). The first peak, at 1.6 Å, is partially due to Pd–N bonds originating from interaction with the g-C₃N₄ support. Moreover, their intensity relative to Pd–Pd bond increased in the Pd@MO_x/CN (M = Ga, Al, or B) compared with the monometallic Pd/CN. The inverse FT of Pd@GaO_x/CN was well fitted by using Pd–O and Pd–Pd shells, whose interatomic distance (*R*) and coordination number (CN) were determined to be *R* = 2.00 Å and CN = 4.3 and *R* = 2.75 Å and CN = 5.1, respectively (Table 1 and Fig. S4). The contribution of Pd–O bond

Table 1

Curve fitting results determined by Pd K-edge FT-EXAFS data.

	Shell	<i>R</i> / Å	CN	σ ²
Pd@GaO _x /CN	Pd–O	2.00	5.1	0.0069
	Pd–Pd	2.75	5.0	0.0096
Pd@AlO _x /CN	Pd–O	2.01	3.3	0.00660
	Pd–Pd	2.76	5.2	0.0086
Pd@BO _x /CN	Pd–O	2.01	3.1	0.0046
	Pd–Pd	2.76	4.8	0.0055
Pd/CN	Pd–O	2.01	2.5	0.0055
	Pd–Pd	2.76	5.8	0.0076

increased in the order of Pd@GaO_x/CN > Pd@AlO_x/CN ≈ Pd@BO_x/CN > Pd_x/CN. These results suggest that the surfaces of Pd NPs are oxidized by modification with MO_x to some extent. As will be discussed later, curve-fitting results are consistent with the those obtained from CO adsorption, in which the exposed Pd dispersion decreased in the order of Pd@GaO_x/CN < Pd@AlO_x/CN ≈ Pd@BO_x/CN < Pd_x/CN. No shift of the second Pd–Pd bond was observed for all samples compared with Pd, which may rule out the formation of intermetallic alloy compounds.

The shape of the Ga K-edge XANES spectrum of Pd@GaO_x/CN was intermediate between that of Ga(NO₃)₃·*n*H₂O and Ga₂O₃ (Fig. 1c). The FT-EXAFS spectrum of Pd@GaO_x/CN exhibited two peaks at approximately 1.6 and 2.5 Å due to the Ga–O bond and Ga–O–Ga bond, respectively (Fig. 1d). The intensity of the second peak in the spectrum of Pd@GaO_x/CN was slightly weaker than that in the reference spectrum of Ga₂O₃. The reduced intensity in this region can be explained by the formation of structurally disordered NPs of extremely small size [40]. Additionally, the Ga–O–Ga bond in the spectrum of Pd@GaO_x/CN was slightly shifted to a longer interatomic distance than that of Ga₂O₃, which is indicative of the formation of Ga–O–Pd bond. No metallic bonds were observed. Because the reduction potentials of Ga³⁺ ions [*E*⁰ (Ga³⁺/Ga²⁺) = −0.59 V vs. the normal hydrogen electrode (NHE)] are more negative than those of Pd²⁺ ions [*E*⁰ (Pd²⁺/Pd⁰) = +0.99 V vs. NHE], the reduction of Ga³⁺ ions was delayed more than that of Pd²⁺ ions, leading to preferential formation of amorphous MO_x phase on the surface of Pd NPs via Pd–O–Ga bonds.

In the temperature-programmed reduction under hydrogen (H₂-TPR). The peak attributed to the reduction of PdO to metallic Pd observed in Pd/CN was broadened and shifted to a higher temperature in Pd@GaO_x/CN (Fig. S5). This indicates that the GaO_x phase exists in the periphery of the Pd NPs, which influences the reduction sequence of Pd NPs. A high-angle annular dark-field scanning transmission electron microscopy (STEM) image of Pd@GaO_x/CN is shown in Fig. 2a. Energy-dispersive X-ray spectroscopy maps of a selected area demonstrate that the white particle is composed of Pd and that the Ga atoms are highly dispersed throughout the material (Fig. 2b and c). The mean particle diameter (*d*_{ave}) was determined to be 6.3 nm (Fig. 2d). This value is comparable with that obtained for Pd/CN (*d*_{ave} = 5.3 nm), Pd@AlO_x/CN (*d*_{ave} = 6.5 nm), and Pd@BO_x/CN (*d*_{ave} = 6.8 nm), as summarized in Fig. S6. The elemental distribution across the surface of a single NP provided strong evidence that Ga atoms occur in the periphery of Pd NPs (Fig. 2e). More detailed investigation suggests that Pd NPs exposed Pd (111) with a d-spacing of 0.224 nm (Fig. 2f and g), while no crystal phase was observed in its periphery despite Ga atoms being confirmed by EDX (Fig. 2h). By considering these results as well as the differences in reduction potential between Pd²⁺ and Ga³⁺, a possible structure was proposed, in which amorphous GaO_x phases were partially located on the surfaces of Pd NPs, as illustrated in Fig. 2i.

In an effort to investigate the influence of GaO_x phase on the electronic state of the active Pd species, atomic charges were calculated using DFT. Here we considered supercell slab models consisting of a surface 5 × 5 surface unit cells including Pd(111) interacting with a M₂O₃ cluster (M = Ga, Al, or B). The optimized structure of Pd(111) associated with a single stoichiometric Ga₂O₃ cluster is shown in Fig. 3A (a). The colors of Pd atoms in this figure refer to their calculated

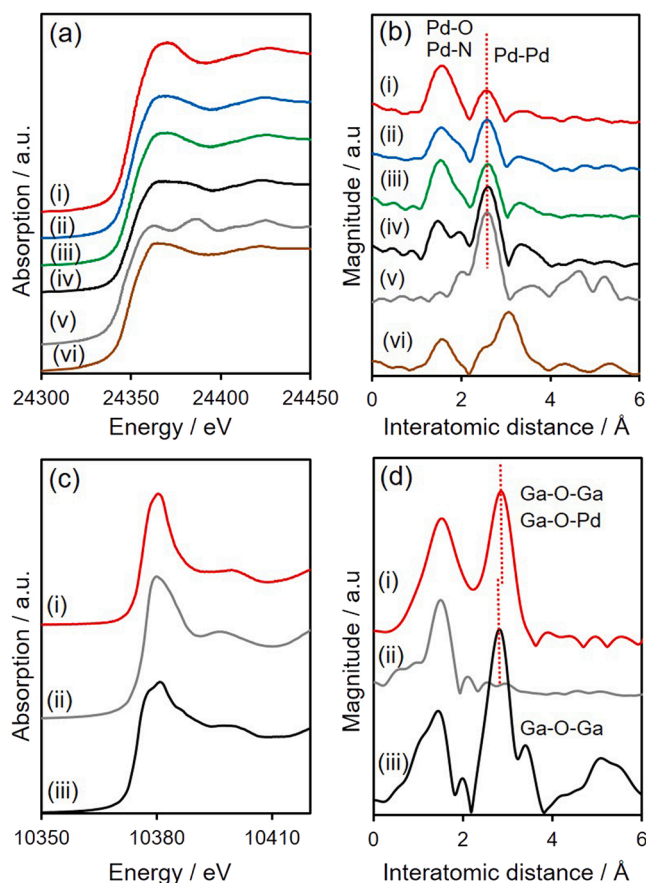


Fig. 1. (a) Pd K-edge X-ray absorption near-edge structure (XANES) and (b) Fourier-transform extended X-ray absorption fine structure (FT-EXAFS) spectra of (i) Pd@GaO_x/CN, (ii) Pd@AlO_x/CN, (iii) Pd@BO_x/CN, (iv) Pd/CN, (v) Pd foil, and (vi) PdO. (c) Ga K-edge XANES and (d) FT-EXAFS spectra of (i) Pd@GaO_x/CN, (ii) Ga(NO₃)₃, and (iii) Ga₂O₃.

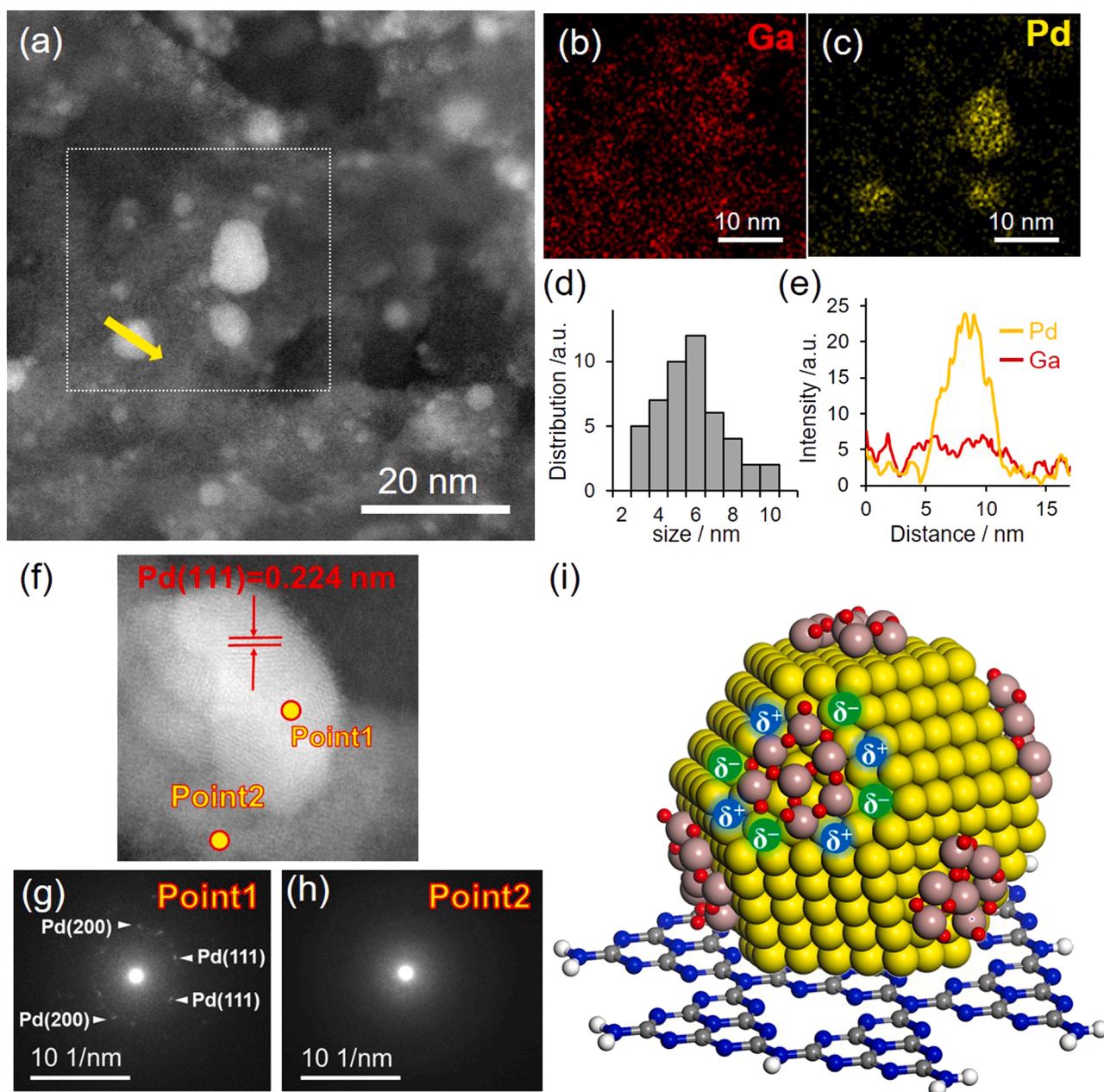


Fig. 2. (a) A HAADF-STEM image of Pd@GaO_x/CN. (b, c) EDS maps for (b) Ga and (c) Pd. (d) Size distribution of nanoparticles determined from STEM image. (e) Cross-sectional EDS line profile obtained from a single nanoparticle in Fig. 2a. (f) HAADF-STEM image in the other area, (g, h) electron diffraction patterns of Point 1 and point 2 in (f). (i) Structural model of Pd@GaO_x/CN.

Mulliken atomic charges. This analysis demonstrated that an electron is transferred from the Ga atom of Ga₂O₃ to a nearby Pd atom. The four green Pd atoms in the periphery of the Ga atom were strongly negatively charged. In contrast, the blue Pd atoms bounded by the O atoms of Ga₂O₃ were positively charged, indicating electron transfer from the Pd atoms to the O atoms. Such electronic interaction generates the unique Pd ensemble sites where electron-deficient Pd^{δ+} and electron-rich Pd^{δ-} are adjacent. A similar tendency can be observed in the case of Pd(111) associated with one stoichiometric Al₂O₃ (Fig. 3A(b)) or B₂O₃ (Fig. 3A(c)) cluster; the Pd atoms in the vicinity of the B atom were negatively charged, whereas the Pd atoms connected with the O atoms were positively charged. However, the degrees of positivity and negativity observed in the presence of the B₂O₃ cluster were smaller than those observed in the presence of the Ga₂O₃ or Al₂O₃ cluster. This phenomenon can be explained by the small electronegativities of Ga (1.81) and Al

(1.61) compared with those of B (2.04), causing electron transfer from Ga or Al to Pd (2.20) to be better facilitated than that from B. In the preliminary calculation of Density of State (DOS) values, *d*-band center of Pd(111) + Ga₂O₃ was found to be located at −2.05 eV, which is almost similar to the value of −2.01 eV for Pd (111) (Fig. 3B). This indicates that GaO_x modification does not ameliorate the electronic structure in the bulk, but causes uneven charge distribution on their surface. These results were further evidenced by XPS spectra. The shift of the Pd 3d peaks generated by Pd@GaO_x/CN to lower binding energy was limited to only 0.15 eV compared with that obtained from the monometallic Pd/CN (Fig. S7), presumably because the uneven charge distribution at the quite limited area (adjacent electron-deficient Pd^{δ+} and electron-rich Pd^{δ-}) is averaged and is not reflected in XPS spectra.

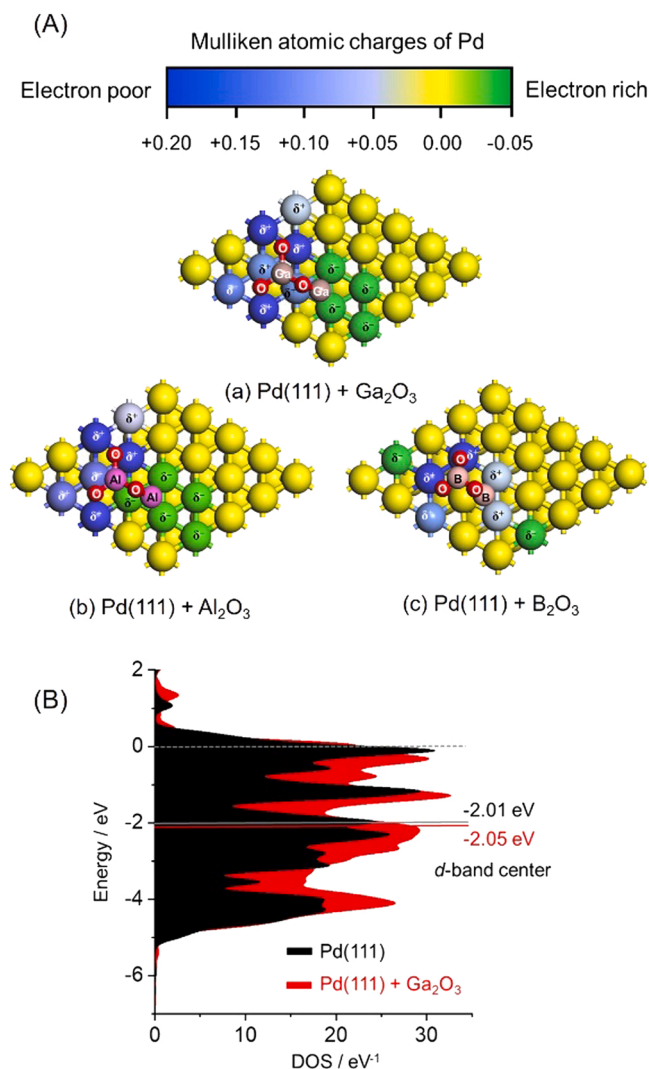


Fig. 3. (A) The optimized structure of Pd(111) associated with one stoichiometric cluster of (a) Ga₂O₃, (b) Al₂O₃, and (c) B₂O₃ with a color overlay of representative Mulliken atomic charge determined using density functional theory calculations. (B) Calculated DOS plots.

3.2. Catalytic and mechanistic investigation of CO₂ hydrogenation

Catalytic activity in CO₂ hydrogenation to formate was examined using a series of Pd-based catalysts, with results shown in Fig. 4a. A typical reaction was performed in a basic aqueous solution containing 1.0 M NaHCO₃ under a total pressure of 2.0 MPa (H₂:CO₂ = 1:1) at 100 °C over 6 h. Comparing the TON values based on the total quantities of Pd employed, Pd@MO_x/CN (M = Ga, Al, or B) exhibited a TON value comparable with or higher than that of monometallic Pd/CN despite the low density of surface-exposed Pd atoms on Pd@MO_x/CN, in which activity increased in the order of Pd@GaO_x/CN < Pd@AlO_x/CN < Pd@BO_x/CN. In an effort to elucidate the potential activity, the dispersion of Pd species was determined using pulsed CO adsorption measurements (Table S1). Since the exposed Pd dispersion of Pd@GaO_x/CN is only 6.5%, a maximum TON value of 4540 (yield of FA = 0.012 mol·h⁻¹·g_{cat}⁻¹) was obtained for Pd@GaO_x/CN based on the quantity of surface-exposed Pd atoms, representing a more than sixfold increase compared with monometallic Pd/CN. FA was obtained with > 99% selectivity and any other products were not observed. The catalytic activity is comparable to and better than some of the previously reported systems (Table S2). The differences in MO_x coverage may be attributed to the affinity between the Pd and a group 13 element. No

other byproducts were found in either liquid or gas phase for any catalyst employed. Notably, Pd/Ga₂O₃ prepared using the same impregnation method, followed by NaBH₄ reduction, showed almost no catalytic activity, indicating that Ga₂O₃ itself does not act as an efficient support. The composition of the Pd@GaO_x/CN catalyst was tuned simply by varying the initial molar ratio of the metal precursors. The effect of Ga content on the TON based on the quantity of surface-exposed Pd atoms is shown in Fig. 4b, in which activity was maximized at Ga = 40 at %. Such precipitously peaked activity order based on the Pd/Ga composition clearly suggests that the synergistic effect originated from the integration of Pd with Ga and that the excess GaO_x may suppress the ease of access to the active Pd centers.

Furthermore, the CO₂ hydrogenation reaction under additive-free aqueous conditions (CO₂ (aq.) + H₂ (aq.) → HCOOH (aq.), ΔG = -4 kJ mol⁻¹) is recently highly desired from an industrial perspective. The Pd@GaO_x/CN displayed high activity (TON=59 at 24 h, TOF=2.5 h⁻¹) in the FA production under additive-free aqueous conditions (that is, in distilled water) with a total pressure of 4.0 MPa (H₂/CO₂ = 1:1) at 40 °C. The attained activity is comparable to and better than some of the previously reported systems, such as PdNi/carbon nanotube (TOF = 0.2 h⁻¹) [8], Pd/g-C₃N₄ (1.5 h⁻¹) [41], and Pd/C₃N₄ with edge defect (TOF = 2.4 h⁻¹) [42], respectively.

A possible reaction mechanism for CO₂ hydrogenation to formate over supported metal NPs, taking into account previous studies, is proposed in Fig. 5a [43–45]. First, the dissociation of H₂ is initiated, yielding a metal hydride species (*step 1*). This is followed by the adsorption of HCO₃⁻, which is transformed from gaseous CO₂ under basic aqueous solutions (*step 2*). Next, dissociated active H atoms attack C atoms of adsorbed HCO₃⁻ ions to give a formate intermediate (*step 3*). The reduction of HCO₃⁻ is energetically more likely to proceed by the attack of active H on the C atom rather than on the O atoms. Finally, the O atom of the OH group undergoes attack by another H atom (*step 4*), leading to the production of formate and H₂O (*step 5*), regenerating the initial active species.

In the reaction under a flow of H₂ and D₂ through the catalyst, the formation rate of HD was significantly enhanced by Pd@MO_x/CN (M = Ga, Al, or B) compared with Pd/CN, and Pd@GaO_x/CN was the most active among the investigated systems, as shown in Fig. 4c. This finding is consistent with the order of catalytic activity in CO₂ hydrogenation. This alignment demonstrates that the addition of group 13 elements promotes dissociation of hydrogen on NP surfaces (*step 1*) [46].

Moreover, the effect of HCO₃⁻ concentration was also critically dependent on the catalyst composition (Fig. 4d–g). All Pd@MO_x/CN catalysts displayed higher reaction orders (Ga, 0.71; Al, 0.74; B, 0.67) than Pd/CN (0.60), as determined using the slope obtained at low HCO₃⁻ concentration. This means the HCO₃⁻ adsorption step is enhanced by interfacial modification. It should be further noted that Pd@GaO_x/CN showed a linear relationship between TON and the HCO₃⁻ concentration across the full range of values. Activity increases with increasing HCO₃⁻ concentration without saturation because the subsequent reaction of the adsorbed HCO₃⁻ species (*step 3*) occurs smoothly over Pd@GaO_x/CN. In contrast, TON values were almost constant across high HCO₃⁻ concentrations for each of the other catalysts. These results suggest that the adsorption sites over such catalysts are likely to be saturated because of the delay of the subsequent reaction of the adsorbed HCO₃⁻ species.

To better understand the positive effect of interfacial MO_x (M = Ga, Al, or B) modification, potential energy profiles were calculated, employing Pd(111) slab models interacting with a M₂O₃ cluster (M = Ga, Al, or B) (Fig. 5b). In the case of Pd(111), H₂ dissociation at Pd sites (*step 1*) is initiated with an activation energy (*E*_a) of 23.8 kcal·mol⁻¹. Next, HCO₃⁻ is adsorbed on Pd to produce intermediate III (*step 2*), with an adsorption energy (*E*_{ad}) determined to be -57.9 kcal·mol⁻¹. Then, reduction takes place through the attack of a hydride ion with an energy barrier of 67.4 kcal·mol⁻¹ (*step 3*). The energy barrier is negligibly small in *step 4*, in which formate is spontaneously generated along with H₂O when the OH of HCO₃⁻ is attacked by another hydride ion. These results

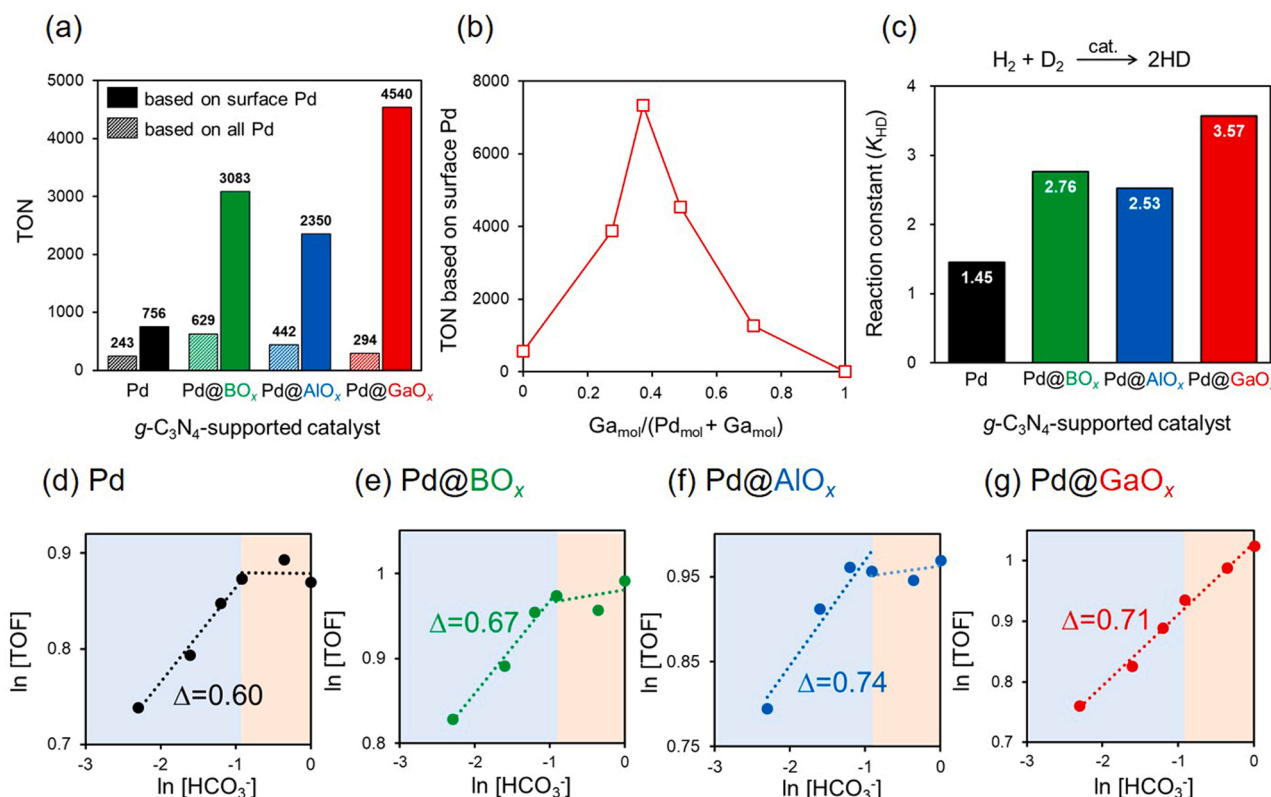


Fig. 4. (a) Comparison of catalytic activity for a series of supported Pd-based catalysts during CO₂ hydrogenation. (b) TON values based on surface Pd atoms versus the atomic fraction of Ga for Pd@GaO_x/CN catalysts of various Pd and Ga concentrations. (c) Comparison of activity during the HD exchange reaction for a series of supported Pd-based catalysts. (d–g) Effect of HCO₃⁻ concentration on TOF values for a series of supported Pd-based catalysts: (d) Pd, (e) Pd@BO_x/CN, (f) Pd@AlO_x/CN, and (g) Pd@GaO_x/CN.

revealed that the rate-determining step in the present catalytic cycle is *step 3*. This is consistent with insights obtained from our previous experimental and theoretical studies [15,16].

In the case of Pd(111) associated with Ga₂O₃, the dissociation of H₂ occurs with an energy barrier of 13.0 kcal·mol⁻¹, which is lower than that obtained for Pd(111) alone. This result agrees with the kinetic data obtained for the HD formation reaction (Fig. 4c). Similarly, the presence of Al₂O₃ and B₂O₃ slightly lowered the *E_a* for H₂ dissociation, as also verified in the kinetic investigations. As discussed above (Fig. 3a), there is an electron transfer from the Ga atoms of Ga₂O₃ to the Pd atoms. This process generates the electron-rich Pd^{δ-}, which facilitates the dissociation of H₂ because the H₂ activation process requires the electron to be injected into the H 1 s antibonding state [47].

The *E_{ad}* values of HCO₃⁻ in *step 2* for Pd(111) interacting with the M₂O₃ cluster (M = Ga, Al, or B) increased in the following order: B (-63.9 kcal·mol⁻¹) < Al (-67.9 kcal·mol⁻¹) < Ga (-72.5 kcal·mol⁻¹). As expected, these values were higher than those for adsorption on pristine Pd(111) (*E_{ad}* = -57.9 kcal·mol⁻¹). This calculation result is in agreement with the effect of HCO₃⁻ concentration on catalytic activity, for which Pd@MO_x/CN catalysts displayed reaction orders higher than those of Pd/CN (Fig. 4d–g). Thus, interfacial modification with group 13 elements plays an important role in the stabilization of HCO₃⁻ ions; in comparison with the situation in pristine Pd(111), the Mulliken atomic charges of Pd atoms bounded by O atoms of M₂O₃ were positively charged by electron transfer from the Pd atoms to the O atoms, and the degrees of positivity and negativity were larger in Ga₂O₃ (Fig. 3). The generation of such electron-deficient Pd^{δ+} accordingly increased the adsorption of HCO₃⁻. This increase further promoted the subsequent reduction of HCO₃⁻ (*step 4*), since the larger *E_{ad}* for the reaction intermediate on the metal catalyst corresponded to a lower reaction barrier according to the Brønsted–Evans–Polanyi relationship [48].

As expected, the *E_a* for the reduction of HCO₃⁻ for Pd(111) interacting with a M₂O₃ cluster (M = Ga, Al, or B) was lower than that for pristine Pd (111), and more significant enhancement of this step was observed for Pd(111) interacting with a M₂O₃ cluster than for pristine Pd(111). These results are also in good agreement with our kinetic investigation into the effect of HCO₃⁻ concentration. In that context, the catalytic activity increased with increasing HCO₃⁻ concentration without saturation even at high concentrations. These results further demonstrate that modification with group 13 elements plays a pivotal role in boosting performance at the rate-determining step.

The enhancement in the rate-determining step can be explained by considering the electronic state in reaction intermediate III in Fig. 5a. DFT-optimized configurations are summarized in Fig. 6. The C atoms of the adsorbed HCO₃⁻ ions at an electron-deficient Pd^{δ+} site over Pd(111) interacting with a Ga₂O₃ cluster are more positively charged than elsewhere, as shown in Table 1. In contrast, the electronic charges of the dissociated hydride species at an electron-rich Pd^{δ-} site are negative. Therefore, the more strongly positive C atoms of the adsorbed HCO₃⁻ ions are the most likely carbon atoms to undergo attack by the dissociated hydride species. It can thus be concluded that the electronic effect resulting from the interplay of the Pd ensemble sites induced by GaO_x modification explains the enhanced activity during CO₂ hydrogenation. With respect to the above-mentioned mechanism, we also point out the participation of multiple interactions at the metal/support interface [49, 50]. The interaction of HCO₃⁻ with g-C₃N₄ support via the formation of O–H···N hydrogen bonds give rise to the positively polarized carbon in HCO₃⁻, which easily undergoes the attacks by the dissociated H atom at Pd accompanied by the simultaneous formation of the formate intermediate. The electron density transfer from the semiconductor g-C₃N₄ to Pd NPs in the heterojunction also plays an important role in the formation of electronically enriched metallic Pd [49] Table 2.

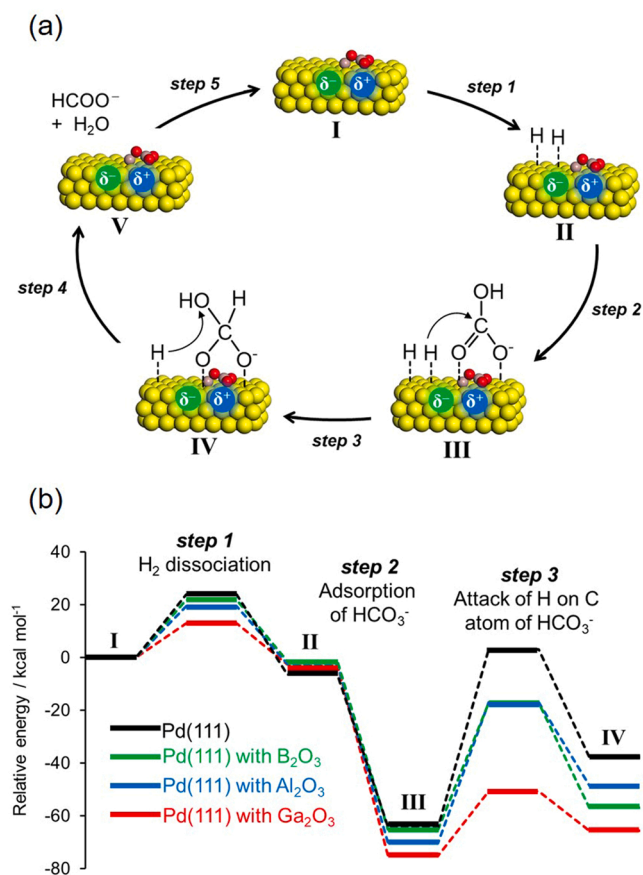


Fig. 5. (a) Possible reaction mechanism for the hydrogenation of CO₂ to formate and (b) the corresponding potential energy profiles as determined using density functional theory calculations for Pd (111) and Pd(111) associated with a M₂O₃ cluster (M = Ga, Al, or B).

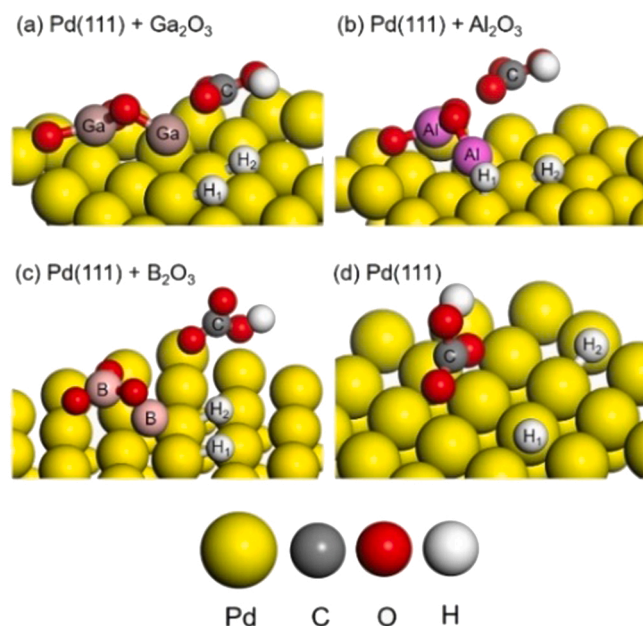


Fig. 6. DFT-optimized configurations for dissociated H atoms and HCO₃⁻ ions adsorbed on (a, b, and c) PdAg (111) associated with an M₂O₃ (M = Ga, Al, or B) and (d) PdAg (111).

Table 2

Adsorption energy values (E_{ad}) for HCO₃⁻ and representative Mulliken atomic charges as determined using density functional theory calculations involving the reaction intermediates in the rate-determining steps for bare Pd(111) and Pd (111) associated with the M₂O₃ cluster (M = Ga, Al, or B).

Sample	E_{ad} of HCO ₃ ⁻ (kcal·mol ⁻¹)	Atomic charge		
		C atom of HCO ₃ ⁻	H atom	
			H ₁	H ₂
Pd(111)	-72.5	0.734	-0.029	-0.003
+ Ga ₂ O ₃				
Pd(111)	-67.9	0.675	-0.006	-0.059
+ Al ₂ O ₃				
Pd(111)	-63.9	0.666	0.002	-0.019
+ B ₂ O ₃				
Pd(111)	-57.9	0.668	-0.031	-0.018

4. Conclusions

We successfully achieved enhanced activity of a Pd-based catalyst during CO₂ hydrogenation to FA via interfacial modification with highly dispersed amorphous MO_x phase (M = Ga, Al, or B). In particular, the activity of Pd@GaO_x/CN was enhanced sixfold relative to that of monometallic Pd/CN based on the quantity of surface-exposed Pd atoms. Dual activation of hydrogen and HCO₃⁻ over ensemble Pd sites was elucidated by kinetics data and DFT calculations. The electron-deficient Pd^{δ+} species associated with O atoms of Ga₂O₃ enhanced the adsorption energy of HCO₃⁻ ions, whereas the electron-rich Pd^{δ-} species in the periphery of the Ga atom promoted H₂ dissociation as well as the attack of dissociated H atoms on C atoms in HCO₃⁻ ions. This study thus provides key information on the advanced design of catalytic active centers for CO₂ hydrogenation to FA. The findings also emphasize the importance of interface design for further improvement of catalytic performance, resulting in a key practical application: the realization of a reversible, environmentally friendly hydrogen storage system mediated by CO₂ and FA.

CCRediT authorship contribution statement

Kohsuke Mori: Conceptualization, Supervision, Writing – original draft preparation, Validation. **Hiroto HATA:** Visualization, Investigation, Validation. **Hiromi Yamashita:** Supervision.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Data Availability

No data was used for the research described in the article.

Acknowledgements

The present work was financially supported by TOYOTA Mobility foundation (TMF). Part of this work was supported by the Kakenhi Grant-in-Aid for Transformative Research Areas(B)(No. 21B206), the Japan Society for the Promotion of Science (JSPS, Element Strategy Initiative of MEXT, Japan (no. JPMXP0112101003), and “Dynamic Alliance for Open Innovation Bridging Human, Environment and Materials” from MEXT. A part of the experiments was carried out by using a facility in the Research Center for Ultra-High Voltage Electron Microscopy, Osaka University. The synchrotron radiation experiments for XAFS measurements were performed at the BL01B1 beamline in SPring-8 with the approval from JASRI (2020A1062 and 2021A1095).

Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at [doi:10.1016/j.apcatb.2022.122022](https://doi.org/10.1016/j.apcatb.2022.122022).

References

- [1] E.V. Kondratenko, G. Mul, J. Baltusaitis, G.O. Larrazabal, J. Perez-Ramirez, Status and perspectives of CO₂ conversion into fuels and chemicals by catalytic, photocatalytic and electrocatalytic processes, *Energy Environ. Sci.* 6 (2013) 3112–3135.
- [2] P.G. Jessop, T. Ikariya, R. Noyori, Homogeneous hydrogenation of carbon dioxide, *Chem. Rev.* 95 (1995) 259–272.
- [3] S. Enthaler, Carbon dioxide—the hydrogen-storage material of the future? *ChemSusChem* 1 (2008) 801–804.
- [4] S. Enthaler, J. von Langermann, T. Schmidt, Carbon dioxide and formic acid—the couple for environmental-friendly hydrogen storage? *Energy Environ. Sci.* 3 (2010) 1207–1217.
- [5] P. Verma, S. Zhang, S. Song, K. Mori, Y. Kuwahara, M. Wen, H. Yamashita, T. An, Recent strategies for enhancing the catalytic activity of CO₂ hydrogenation to formate/formic acid over Pd-based catalyst, *J. CO₂ Util.* 54 (2021), 101765.
- [6] S. Moret, P.J. Dyson, G. Laurenczy, Direct synthesis of formic acid from carbon dioxide by hydrogenation in acidic media, *Nat. Commun.* 5 (2014) 4017.
- [7] P.G. Jessop, F. Joó, C.-C. Tai, Recent advances in the homogeneous hydrogenation of carbon dioxide, *Coord. Chem. Rev.* 248 (2004) 2425–2442.
- [8] L.T.M. Nguyen, H. Park, M. Banu, J.Y. Kim, D.H. Youn, G. Magesh, W.Y. Kim, J. S. Lee, Catalytic CO₂ hydrogenation to formic acid over carbon nanotube-graphene supported PdNi alloy catalysts, *RSC Adv.* 5 (2015) 105560–105566.
- [9] D. Mellmann, P. Sponholz, H. Junge, M. Beller, Formic acid as a hydrogen storage material - development of homogeneous catalysts for selective hydrogen release, *Chem. Soc. Rev.* 45 (2016) 3954–3988.
- [10] K. Sordakis, C. Tang, L.K. Vogt, H. Junge, P.J. Dyson, M. Beller, G. Laurenczy, Homogeneous catalysis for sustainable hydrogen storage in formic acid and alcohols, *Chem. Rev.* 118 (2018) 372–433.
- [11] D. Mellmann, P. Sponholz, H. Junge, M. Beller, Formic acid as a hydrogen storage material – development of homogeneous catalysts for selective hydrogen release, *Chem. Soc. Rev.* 45 (2016) 3954–3988.
- [12] A. Álvarez, A. Bansode, A. Urakawa, A.V. Bavykina, T.A. Wezendonk, M. Makkee, J. Gascon, F. Kapteijn, Challenges in the greener production of formates/formic acid, methanol, and DME by heterogeneously catalyzed CO₂ hydrogenation processes, *Chem. Rev.* 117 (2017) 9804–9838.
- [13] K. Mori, T. Taga, H. Yamashita, Isolated single-atomic Ru catalyst bound on a layered double hydroxide for hydrogenation of CO₂ to formic acid, *ACS Catal.* 7 (2017) 3147–3151.
- [14] G.H. Gunasekar, K. Park, K.-D. Jung, S. Yoon, Recent developments in the catalytic hydrogenation of CO₂ to formic acid/formate using heterogeneous catalysts, *Inorg. Chem. Front.* 3 (2016) 882–895.
- [15] K. Mori, T. Sano, H. Kobayashi, H. Yamashita, Surface engineering of a supported PdAg catalyst for hydrogenation of CO₂ to formic acid: elucidating the active Pd atoms in alloy nanoparticles, *J. Am. Chem. Soc.* 140 (2018) 8902–8909.
- [16] K. Mori, A. Konishi, H. Yamashita, Interfacial engineering of PdAg/TiO₂ with a metal-organic framework to promote the hydrogenation of CO₂ to formic acid, *J. Phys. Chem. C* 124 (2020) 11499–11505.
- [17] K. Mori, H. Yamashita, Progress in design and architecture of metal nanoparticles for catalytic applications, *Phys. Chem. Chem. Phys.* 12 (2010) 14420–14432.
- [18] K. Mori, N. Hashimoto, N. Kamiuchi, H. Yoshida, H. Kobayashi, H. Yamashita, Hydrogen spillover-driven synthesis of high-entropy alloy nanoparticles as a robust catalyst for CO₂ hydrogenation, *Nat. Commun.* 12 (2021) 3884.
- [19] C. Xie, Z. Niu, D. Kim, M. Li, P. Yang, Surface and interface control in nanoparticle catalysis, *Chem. Rev.* 120 (2020) 1184–1249.
- [20] P. Paalanen, B.M. Weckhuysen, M. Sankar, Progress in controlling the size, composition and nanostructure of supported gold-palladium nanoparticles for catalytic applications, *Catal. Sci. Tech.* 3 (2013) 2869–2880.
- [21] K. Mori, T. Hara, T. Mizugaki, K. Ebitani, K. Kaneda, Hydroxyapatite-supported palladium nanoclusters: a highly active heterogeneous catalyst for selective oxidation of alcohols by use of molecular oxygen, *J. Am. Chem. Soc.* 126 (2004) 10657–10666.
- [22] Q. Zhang, W. Deng, Y. Wang, Effect of size of catalytically active phases in the dehydrogenation of alcohols and the challenging selective oxidation of hydrocarbons, *Chem. Commun.* 47 (2011) 9275–9292.
- [23] B. Roldan Cuenya, Metal nanoparticle catalysts beginning to shape-up, *Acc. Chem. Res.* 46 (2013) 1682–1691.
- [24] Z. Li, S. Ji, Y. Liu, X. Cao, S. Tian, Y. Chen, Z. Niu, Y. Li, Well-defined materials for heterogeneous catalysis: from nanoparticles to isolated single-atom sites, *Chem. Rev.* 120 (2020) 623–682.
- [25] R. Rizo, B. Roldan Cuenya, Shape-controlled nanoparticles as anodic catalysts in low-temperature fuel cells, *ACS Energy Lett.* 4 (2019) 1484–1495.
- [26] L. Wang, L. Wang, X. Meng, F.-S. Xiao, New strategies for the preparation of sinter-resistant metal-nanoparticle-based catalysts, *Adv. Mater.* 31 (2019) 1901905.
- [27] X. Qian, Y. Kuwahara, K. Mori, H. Yamashita, Silver nanoparticles supported on CeO₂-SBA-15 by microwave irradiation possess metal-support interactions and enhanced catalytic activity, *Chem. Eur. J.* 20 (2014) 15746–15752.
- [28] H. Wang, L. Wang, D. Lin, X. Feng, Y. Niu, B. Zhang, F.-S. Xiao, Strong metal-support interactions on gold nanoparticle catalysts achieved through Le Chatelier's principle, *Nat. Catal.* 4 (2021) 418–424.
- [29] L.M. Rossi, J.L. Fiorio, M.A.S. Garcia, C.P. Ferraz, The role and fate of capping ligands in colloiddally prepared metal nanoparticle catalysts, *Dalton Trans.* 47 (2018) 5889–5915.
- [30] T. Yoshii, D. Umemoto, Y. Kuwahara, K. Mori, H. Yamashita, Engineering of surface environment of Pd nanoparticle catalysts on carbon support with pyrene-thiol ligands for semihydrogenation of alkynes, *ACS Appl. Mater. Interfaces* 11 (2019) 37708–37719.
- [31] S. Li, W. Tian, Y. Liu, The ligand effect of atomically precise gold nanoclusters in tailoring catalytic properties, *Nanoscale* 13 (2021) 16847–16859.
- [32] Z.B. Shifrina, V.G. Matveeva, L.M. Bronstein, Role of polymer structures in catalysis by transition metal and metal oxide nanoparticle composites, *Chem. Rev.* 120 (2020) 1350–1396.
- [33] I. Notarfrancesco, F. Fontaine-Vive, S. Antoniotti, Synergy in the catalytic activity of bimetallic nanoparticles and new synthetic methods for the preparation of fine chemicals, *ChemCatChem* 6 (2014) 2784–2791.
- [34] K. Kusada, H. Kitagawa, A route for phase control in metal nanoparticles: a potential strategy to create advanced materials, *Adv. Mater.* 28 (2016) 1129–1142.
- [35] K. Kusada, D. Wu, H. Kitagawa, Metal-based solid-solution alloy nanoparticles: binary to high-entropy alloys (New Aspects of Platinum Group), *Chem. Eur. J.* 26 (2020) 5105–5130.
- [36] S. Masuda, K. Shun, K. Mori, Y. Kuwahara, H. Yamashita, Synthesis of a binary alloy nanoparticle catalyst with an immiscible combination of Rh and Cu assisted by hydrogen spillover on a TiO₂ support, *Chem. Sci.* 11 (2020) 4194–4203.
- [37] K. Mori, D. Tatsumi, T. Iwamoto, Y. Masui, M. Onaka, H. Yamashita, Ruthenium (II)–Bipyridine/NanoC₃N₄ hybrids: tunable photochemical properties by using exchangeable alkali metal cations, *Chem. Asian J.* 13 (2018) 1348–1356.
- [38] B. Delley, An All-Electron, Numerical method for solving the local density functional for polyatomic molecules, *J. Chem. Phys.* 92 (1990) 508–517.
- [39] B. Delley, From molecules to solids with the DMol³ approach, *J. Chem. Phys.* 113 (2000) 7756–7764.
- [40] S.-T. Wong, J.-F. Lee, S. Cheng, C.-Y. Mou, In-situ study of MCM-41-supported iron oxide catalysts by XANES and EXAFS, *Appl. Catal. A Gen.* 198 (2000) 115–126.
- [41] H. Park, J.H. Lee, E.H. Kim, K.Y. Kim, Y.H. Choi, D.H. Youn, J.S. Lee, A highly active and stable palladium catalyst on a g-C₃N₄ support for direct formic acid synthesis under neutral conditions, *Chem. Commun.* 52 (2016) 14302–14305.
- [42] C. Mondelli, B. Puértolas, M. Ackermann, Z. Chen, J. Pérez-Ramírez, Enhanced base-free formic acid production from CO₂ on Pd/g-C₃N₄ by tuning of the carrier defects, *ChemSusChem* 11 (2018) 2859–2869.
- [43] G.A. Filonenko, W.L. Vrijburg, E.J.M. Hensen, E.A. Pidko, On the activity of supported Au catalysts in the liquid phase hydrogenation of CO₂ to formates, *J. Catal.* 343 (2016) 97–105.
- [44] S. Masuda, K. Mori, Y. Futamura, H. Yamashita, PdAg nanoparticles supported on functionalized mesoporous carbon: promotional effect of surface amine groups in reversible hydrogen delivery/storage mediated by formic acid/CO₂, *ACS Catal.* 8 (2018) 2277–2285.
- [45] C.-S. He, L. Gong, J. Zhang, P.-P. He, Y. Mu, Highly selective hydrogenation of CO₂ into formic acid on a nano-Ni catalyst at ambient temperature: process, mechanisms and catalyst stability, *J. CO₂ Util.* 19 (2017) 157–164.
- [46] L. Bai, X. Wang, Q. Chen, Y. Ye, H. Zheng, J. Guo, Y. Yin, C. Gao, Explaining the size dependence in platinum-nanoparticle-catalyzed hydrogenation reactions, *Angew. Chem. Int. Ed.* 55 (2016) 15656–15661.
- [47] Z. Wei, J. Wang, S. Mao, D. Su, H. Jin, Y. Wang, F. Xu, H. Li, Y. Wang, In situ-generated CoO-Co₃O₄/N-doped carbon nanotubes hybrids as efficient and chemoselective catalysts for hydrogenation of nitroarenes, *ACS Catal.* 5 (2015) 4783–4789.
- [48] M. Tang, J. Deng, M. Li, X. Li, H. Li, Z. Chen, Y. Wang, 3d-Interconnected hierarchical porous N-doped carbon supported ruthenium nanoparticles as an efficient catalyst for toluene and quinoline hydrogenation, *Green Chem.* 18 (2016) 6082–6090.
- [49] X. Shao, J. Xu, Y. Huang, X. Su, H. Duan, X. Wang, T. Zhang, Pd/C₃N₄ nanocatalyst for highly efficient hydrogen storage system based on potassium bicarbonate/formate, *AIChE J.* 62 (2016) 2410–2418.
- [50] J.H. Lee, J. Ryu, J.Y. Kim, S.-W. Nam, J.H. Han, T.-H. Lim, S. Gautam, K.H. Chae, C.W. Yoon, Carbon dioxide mediated, reversible chemical hydrogen storage using a Pd nanocatalyst supported on mesoporous graphitic carbon nitride, *J. Mater. Chem. A* 2 (2014) 9490–9495.